

Serial No. 09/700,367

KARER et al.

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## A P P E N D I X I:

CLAIM AMENDMENTS:

Amend Claim 1, and enter new Claims 16 to 22, as indicated in the following listing of the claims:

1. (currently amended) A gas-phase fluidized-bed reactor for polymerizing ethylenically unsaturated monomers, which comprises

- a reactor chamber (1) in the form of a vertical tube which has a region of transition in the lower section of the tube, followed by a reaction zone which is followed by a calming zone (2) in the upper section of the tube,

- a circulation gas line (3) which is connected to the upper section and the lower section of the reactor chamber and is adapted to convey a reaction gas from the calming zone to the region of transition, and

- a circulation gas compressor (4) and a cooling device (5), the circulation gas compressor (4) and the cooling device (5) being sited in the circulation gas line (3),

wherein the region of transition is adapted for transitioning the reaction gas from the circulation gas line into the reactor chamber, and wherein ~~the reactor chamber has~~ in the region of transition, is designed such that either no gas distributor plate is present, or has such that only a gas distributor plate is present which has having a total surface area and has gas orifices, which and wherein said gas orifices occupy more than 50% of the total surface area of said gas distributor plate, and

wherein the gas-phase fluidized-bed reactor has no internal heat exchanger in the reactor chamber.

2. (original) A reactor as claimed in claim 1, wherein there is no gas distributor plate in the region of transition of the reaction gas from the circulation gas line into the reactor chamber or in the lower section of the reactor chamber itself.
3. (original) A reactor as claimed in claim 1, wherein, in the region of transition of the reaction gas from the circulation gas line into the reactor chamber or in the lower section of the reactor chamber itself, there is a gas distributor plate the total surface area of whose gas orifices is more than 90% of the total surface area of said gas distributor plate.

060717

- 8 -

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Serial No. 09/700,367

KARER et al.

DE000003

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4. (previously presented) A reactor as claimed in claim 1, wherein flow reshapers are sited in the region of transition of the reaction gas from the circulation gas line into the reactor chamber in order to reshape the flow pulse of the incoming gas, said reshapers being arranged so as to bring about substantially homogeneous introduction of the gas flow into the fluidized bed.
  5. (canceled)
  6. (previously presented) A reactor as claimed in claim 1, having an internal diameter of the reactor chamber (1) of more than 0.5 m.
  7. (previously presented) A reactor as claimed in claim 1, which further comprises a closable flap situated in the region of transition from the circulation gas line into the lower section of the reactor chamber which flap is adapted to prevent the penetration of polymer particles into the circulation gas line when the compressor is switched off.
  8. (original) A reactor as claimed in claim 7, wherein the closable flap is provided with uniformly distributed holes having a diameter of between 1 and 7 mm.
  9. (canceled)
  10. (previously presented) A reactor as claimed in claim 1, wherein between the reactor chamber (1) and the compressor (4) and the cooling device (5) of the circulation gas line there is sited a cyclone to separate off polymer and catalyst particles from the circulation gas.
  11. (withdrawn - previously presented) A process for polymerizing ethylene or for copolymerizing ethylene with C<sub>3</sub>- to C<sub>8</sub>- $\alpha$ -olefins, wherein the (co)polymerization is conducted in a reactor as claimed in claim 1.
  12. (withdrawn - previously presented) A process as claimed in claim 11, wherein polymerization is conducted in the presence of condensed monomers and/or condensed hydrocarbons.
  13. (withdrawn - previously presented) A process as claimed in claim 11, wherein a mixture comprising gaseous and liquid monomers is fed into the reactor chamber.
  14. (withdrawn - previously presented) A process as claimed in claim 11, wherein to prepare a (co)polymer of a preselected density d the

060717

- 9 -

Serial No. 09/700,367

KARER et al.

DE000003

(co)polymerization is conducted at a temperature situated within a range bounded by an upper limit of equation (I)

$$T_H = 171 + \frac{6d'}{0.84-d'} \quad (I)$$

and a lower limit of equation (II)

$$T_L = 173 + \frac{7.3d'}{0.837-d'} \quad (II)$$

where

$T_H$  is the highest reaction temperature in °C

$T_L$  is the lowest reaction temperature in °C

$d'$  is the numerical value of the density ( $d$ ) [ $\text{g}/\text{cm}^3$ ] of the (co)polymer to be prepared.

15. (withdrawn - previously presented) A process for preparing EPDM, wherein the copolymerization is conducted in a reactor as claimed in claim 1.
16. (new) A gas-phase fluidized-bed reactor for polymerizing ethylenically unsaturated monomers, which comprises
- a reactor chamber (1) in the form of a vertical tube said reactor chamber consisting essentially of a region of transition in the lower section of the tube, followed by a reaction zone which is followed by a calming zone (2) in the upper section of the tube,
  - a circulation gas line (3) which is connected to the upper section and the lower section of the reactor chamber and is adapted to convey a reaction gas from the calming zone to the region of transition, and
  - a circulation gas compressor (4) and a cooling device (5), the circulation gas compressor (4) and the cooling device (5) being sited in the circulation gas line (3),
- wherein the region of transition is adapted for transitioning the reaction gas from the circulation gas line into the reactor chamber, and wherein the reactor chamber has, in the region of transition, either no gas distributor plate or has a gas distributor plate having a total surface area and gas orifices which occupy

060717

- 10 -

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Serial No. 09/700,367

KARER et al.

DE000003

more than 50% of the total surface area of said gas distributor plate, and wherein the gas-phase fluidized-bed reactor has no internal heat exchanger in the reactor chamber.

17. (new) A reactor as claimed in claim 16, wherein there is no gas distributor plate in the region of transition of the reaction gas from the circulation gas line into the reactor chamber or in the reaction zone of the reactor chamber.

18. (new) A reactor as claimed in claim 16, wherein, in the region of transition of the reaction gas from the circulation gas line into the reactor chamber or in the reaction zone of the reactor chamber, there is a gas distributor plate the total surface area of whose gas orifices is more than 90% of the total surface area of said gas distributor plate.

19. (new) A reactor as claimed in claim 16, wherein flow reshapers are sited in the region of transition of the reaction gas from the circulation gas line into the reactor chamber in order to reshape the flow pulse of the incoming gas, said reshapers being arranged so as to bring about substantially homogeneous introduction of the gas flow into the fluidized bed.

20. (new) A reactor as claimed in claim 16, having an internal diameter of the reactor chamber (1) of more than 0.5 m.

21. (new) A reactor as claimed in claim 16, which further comprises a closable flap situated in the region of transition from the circulation gas line into the lower section of the reactor chamber which flap is adapted to prevent the penetration of polymer particles into the circulation gas line when the compressor is switched off.

22. (new) A reactor as claimed in claim 21, wherein the closable flap is provided with uniformly distributed holes having a diameter of between 1 and 7 mm.

23. (new) A reactor as claimed in claim 16, wherein between the reactor chamber (1) and the compressor (4) and the cooling device (5) of the circulation gas line there is sited a cyclone to separate off polymer and catalyst particles from the circulation gas.

060717

- 11 -

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